

# **Analysis and Design of Linear Control System –Part2-**

Instructor: Prof. Masayuki Fujita

# 5th Lecture

## 12 Robust Performance

### 12.4 Robust Pole Placement: Examples

#### Example 12.8 (Slow Stable Process Zeros)

(pp. 362--364)

#### Example 12.9 (Fast Stable Process Poles)

(pp. 364--365)

**Keyword :** Robust Pole Placement,  
Slow Stable Process Zeros,  
Fast Stable Process Poles

# [Ex. 12.8] Vehicle steering

(Ex. 2.8, 5.12, 7.3, 7.4, 8.6)

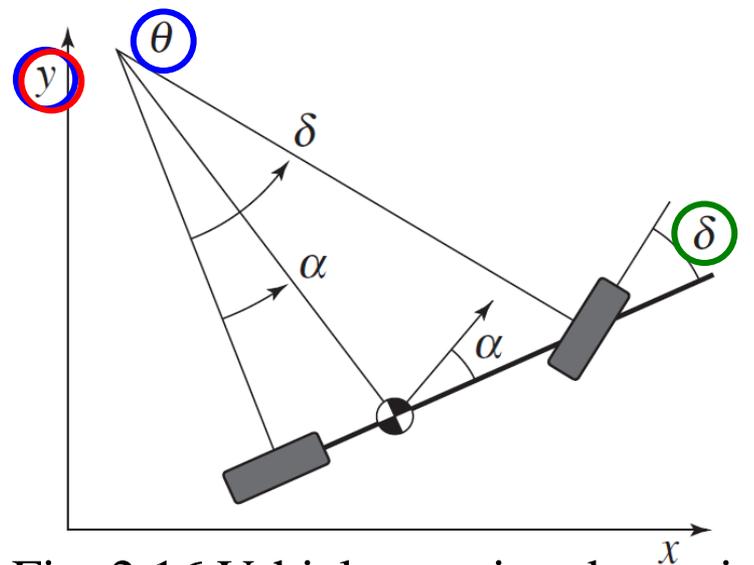
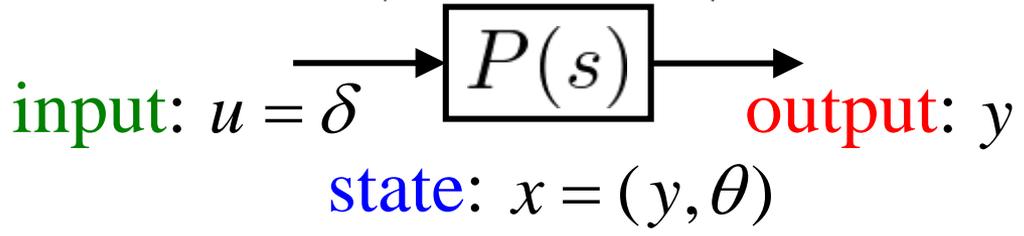
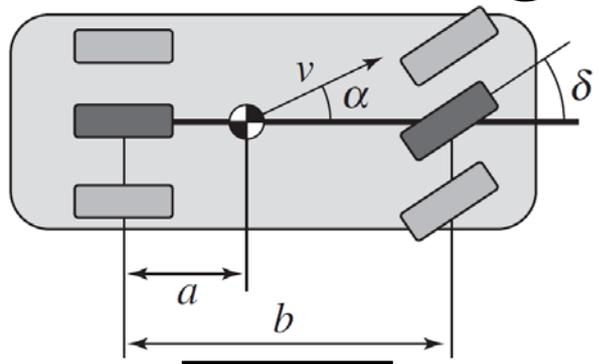


Fig. 2.16 Vehicle steering dynamics

State equation : Plant model ( § 8.3)

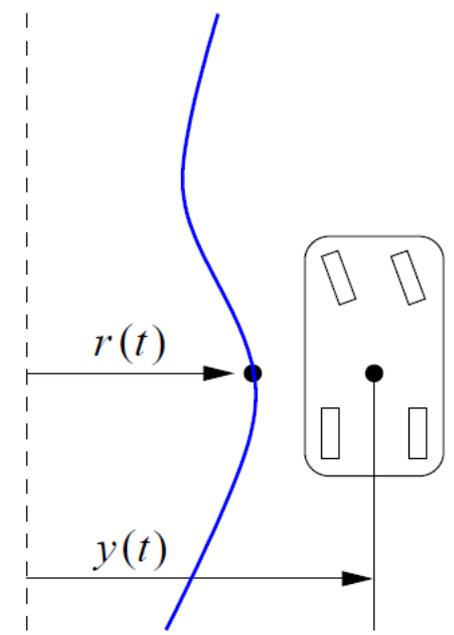
$$\frac{dx}{dt} = Ax + Bu, \quad y = Cx + Du$$

$$A = \begin{bmatrix} 0 & 1 \\ 0 & 0 \end{bmatrix} \quad B = \begin{bmatrix} \gamma \\ 1 \end{bmatrix} \quad C = [1 \quad 0] \quad D = 0$$

$$\gamma = 0.5$$

Transfer function

$$P(s) = C(sI - A)^{-1}B + D = \frac{\gamma s + 1}{s^2}$$



# [Ex. 12.8] Vehicle steering

Controller

Observer

$$\frac{d\hat{x}}{dt} = A\hat{x} + Bu + L(y - C\hat{x})$$

State feedback

$$u = -K\hat{x} + k_r r$$

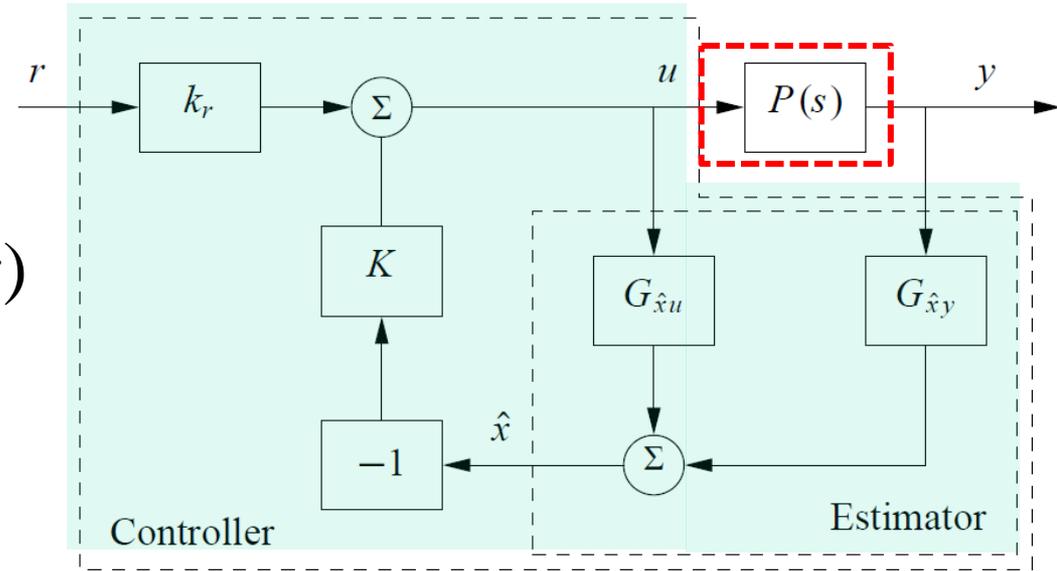


Fig. 8.9 Block diagram for a steering control system

Closed loop system  $\tilde{x} = x - \hat{x}$

$$\frac{d}{dt} \begin{bmatrix} x \\ \tilde{x} \end{bmatrix} = \begin{bmatrix} A - BK & BK \\ 0 & A - LC \end{bmatrix} \begin{bmatrix} x \\ \tilde{x} \end{bmatrix} + \begin{bmatrix} Bk_r \\ 0 \end{bmatrix} r$$

$$y = \begin{bmatrix} C & 0 \end{bmatrix} \begin{bmatrix} x \\ \tilde{x} \end{bmatrix}$$

$$\lambda(s) = \det(sI - A + BK) \det(sI - A + LC)$$

**Separation Principle**

# [Ex. 12.8] Vehicle steering

# Pole Placement

## State feedback gain

$$\det(sI - A + BK) = s^2 + (\gamma k_1 + k_2)s + k_1$$

$$\downarrow = s^2 + 2\zeta_c \omega_c s + \omega_c^2$$

$$k_1 = \omega_c^2 \quad k_2 = 2\zeta_c \omega_c - \gamma \omega_c^2$$

## Observer gain

$$\det(sI - A + LC) = s^2 + l_1 s + l_2$$

$$\downarrow = s^2 + 2\zeta_o \omega_o s + \omega_o^2$$

$$l_1 = 2\zeta_o \omega_o \quad l_2 = \omega_o^2$$

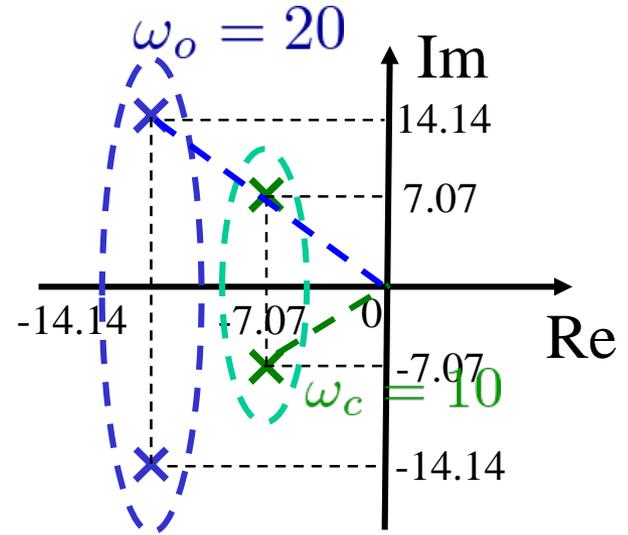
## Faster close loop system

$$\left\{ \begin{array}{ll} \omega_c = 10 & \omega_o = 20 \\ \zeta_c = 0.707 & \zeta_o = 0.707 \end{array} \right.$$

$$-7.07 \pm 7.07i \quad -14.14 \pm 14.14i$$

Should be GOOD?

$$\left\{ \begin{array}{ll} k_1 = 100 & l_1 = 28.28 \\ k_2 = -35.86 & l_2 = 400 \end{array} \right.$$



- × eig. val. of  $A - BK$
- × eig. val. of  $A - LC$

# [Ex. 12.8] Vehicle steering

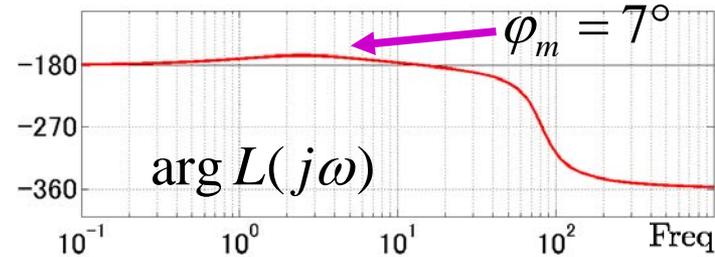
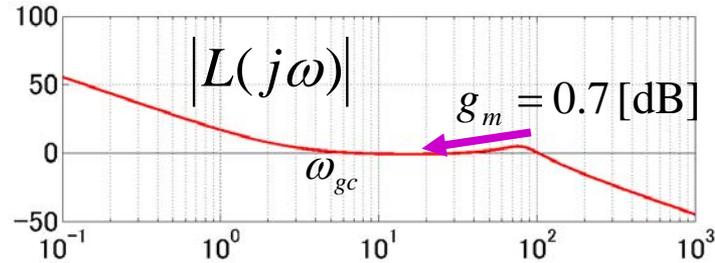
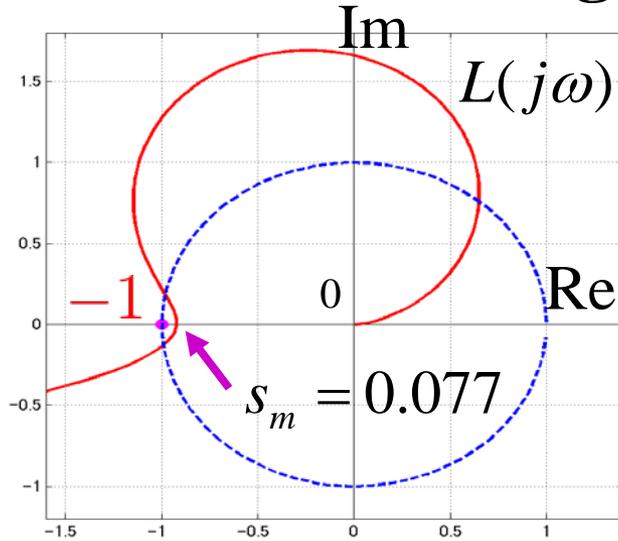


Fig. 12.11

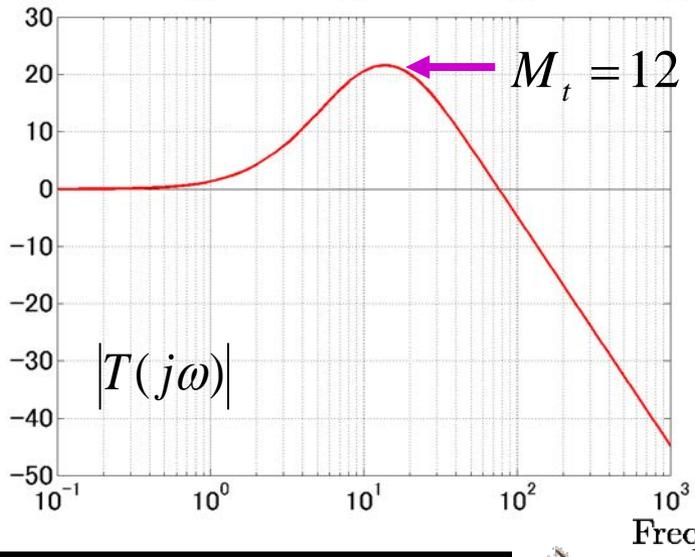
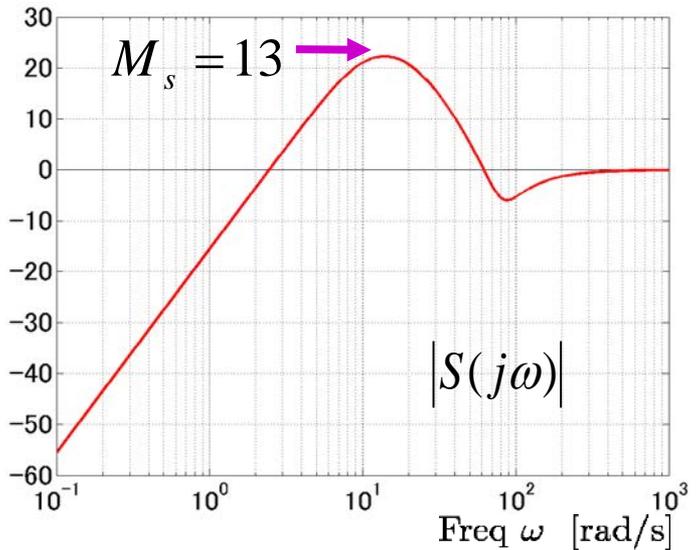
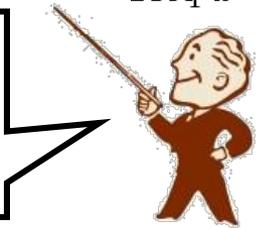


Fig. 12.12

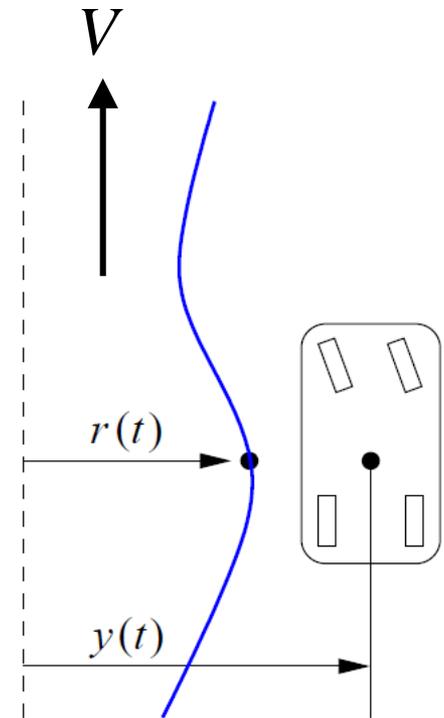
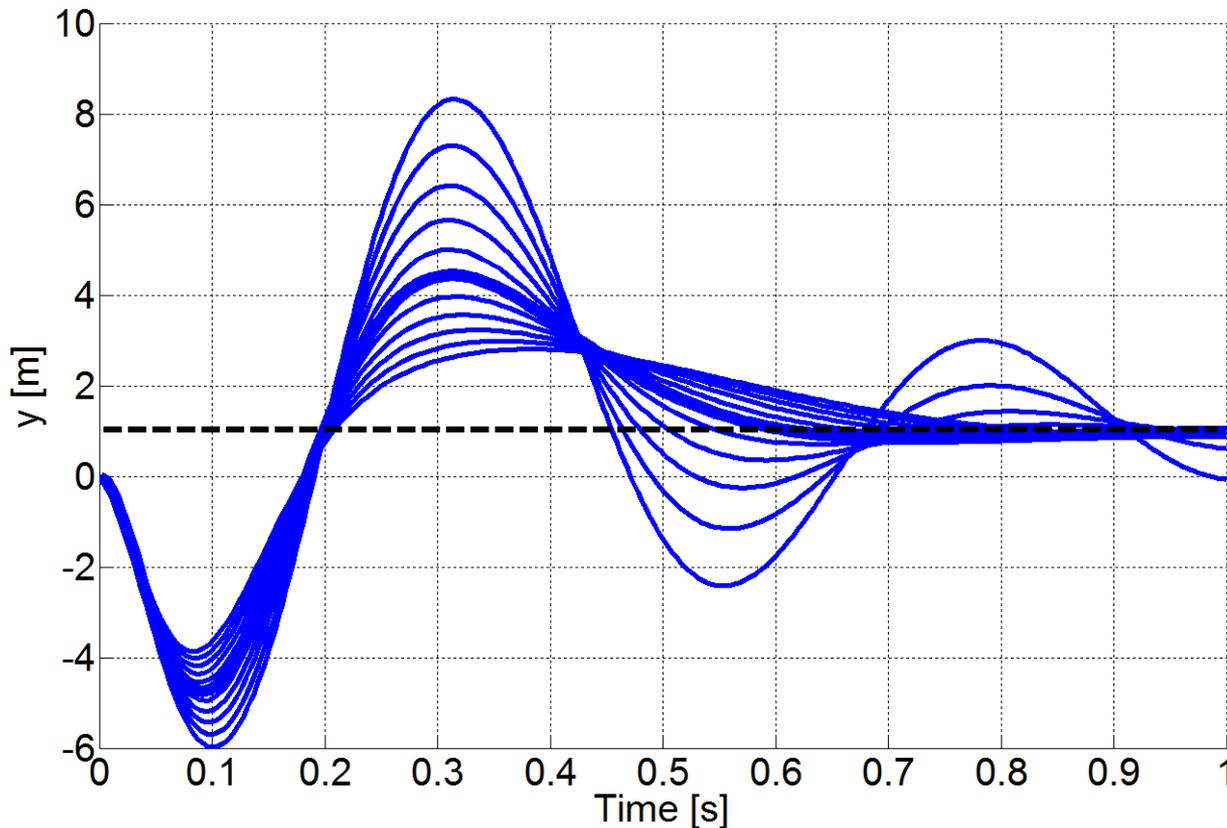
The controller achieves a good control performance, doesn't it?



# [Ex. 12.8] Vehicle steering

$$\left\{ \begin{array}{ll} \omega_c = 10 & \omega_o = 20 \\ \zeta_c = 0.707 & \zeta_o = 0.707 \\ -7.07 \pm 7.07i & -14.14 \pm 14.14i \end{array} \right.$$

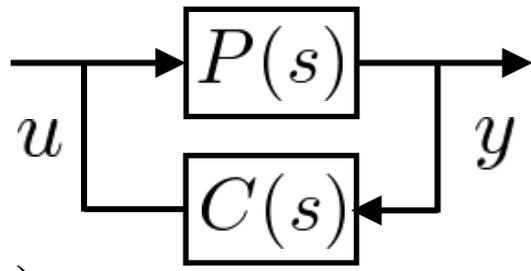
**Nominal**  $V = 1$   
**Variation**  $0.95 \leq V \leq 1.05$



**Oops . . . both performance and robust stability are poor !**

# [Ex. 12.8] Slow Stable Process Zeros

**What happens ?**

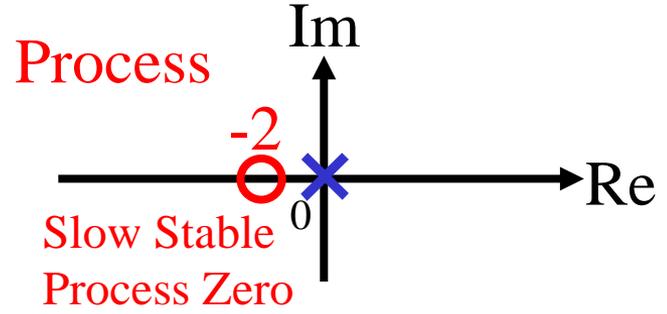


Process (from  $u$  to  $y$ )

$$P(s) = C(sI - A)^{-1}B + D = \frac{\gamma s + 1}{s^2}$$

$$= \frac{0.5s + 1}{s^2}$$

**Pole :**  $p = 0, 0$   
**Zero :**  $z = -2$

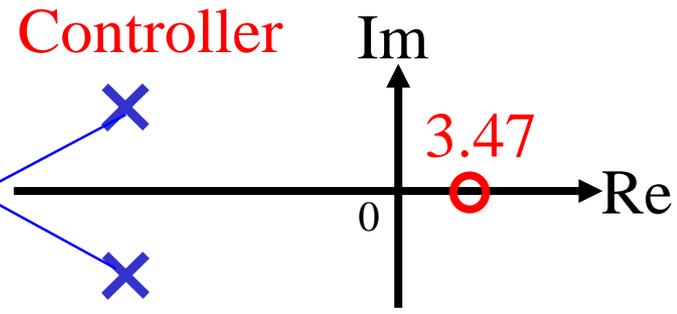


Controller (from  $y$  to  $u$ ) (§ 8.3)

$$C(s) = \frac{KG_{\hat{x}y}(s)}{1 + KG_{\hat{x}u}(s)}$$

$$= \frac{-11516s + 40000}{s^2 + 42.4s + 6657.9}$$

$-21 \pm 79i$   
**Pole :**  $p = -21 \pm 79i$   
**Zero :**  $z = 3.47$



**x Pole**  
**o Zero**

# [Ex. 12.8] Slow Stable Process Zeros

$$T = \frac{PC}{1+PC} = \frac{n_p n_c}{d_p d_c + n_p n_c}$$

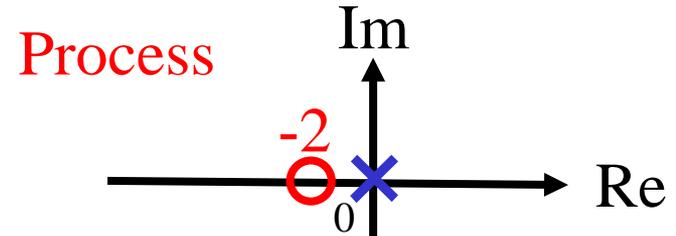
$$P = \frac{n_p}{d_p}, C = \frac{n_c}{d_c}$$

$T$  has the poles of closed-loop system and its zeros are given by **zeros of the process and controller**

Process (from  $u$  to  $y$ )

$$P(s) = \frac{0.5s + 1}{s^2} \leftarrow n_p$$

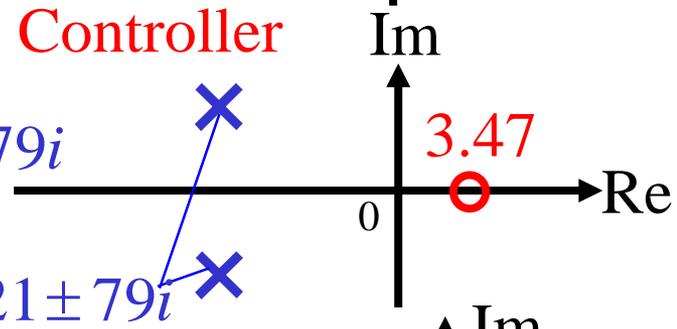
**Pole :**  $p = 0, 0$   
**Zero :**  $z = -2$



Controller (from  $y$  to  $u$ )

$$C(s) = \frac{-11516s + 40000}{s^2 + 42.4s + 6657.9} \leftarrow n_c$$

**Pole :**  $p = -21 \pm 79i$   
**Zero :**  $z = 3.47$

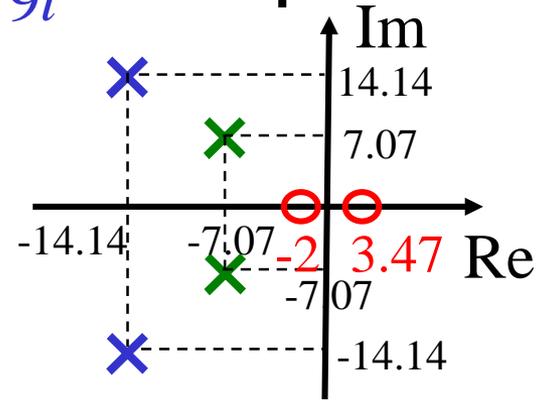


**Closed-loop (from  $r$  to  $y$ )**

$$T(s) = \frac{-5758(s+2)(s-3.47)}{(s^2 + 14.14s + 100)(s^2 + 28s + 400)}$$

**Pole :**  $d_p d_c + n_p n_c = 0$   
 $p = -7.07 \pm 7.07i$   
 $-14.14 \pm 14.14i$

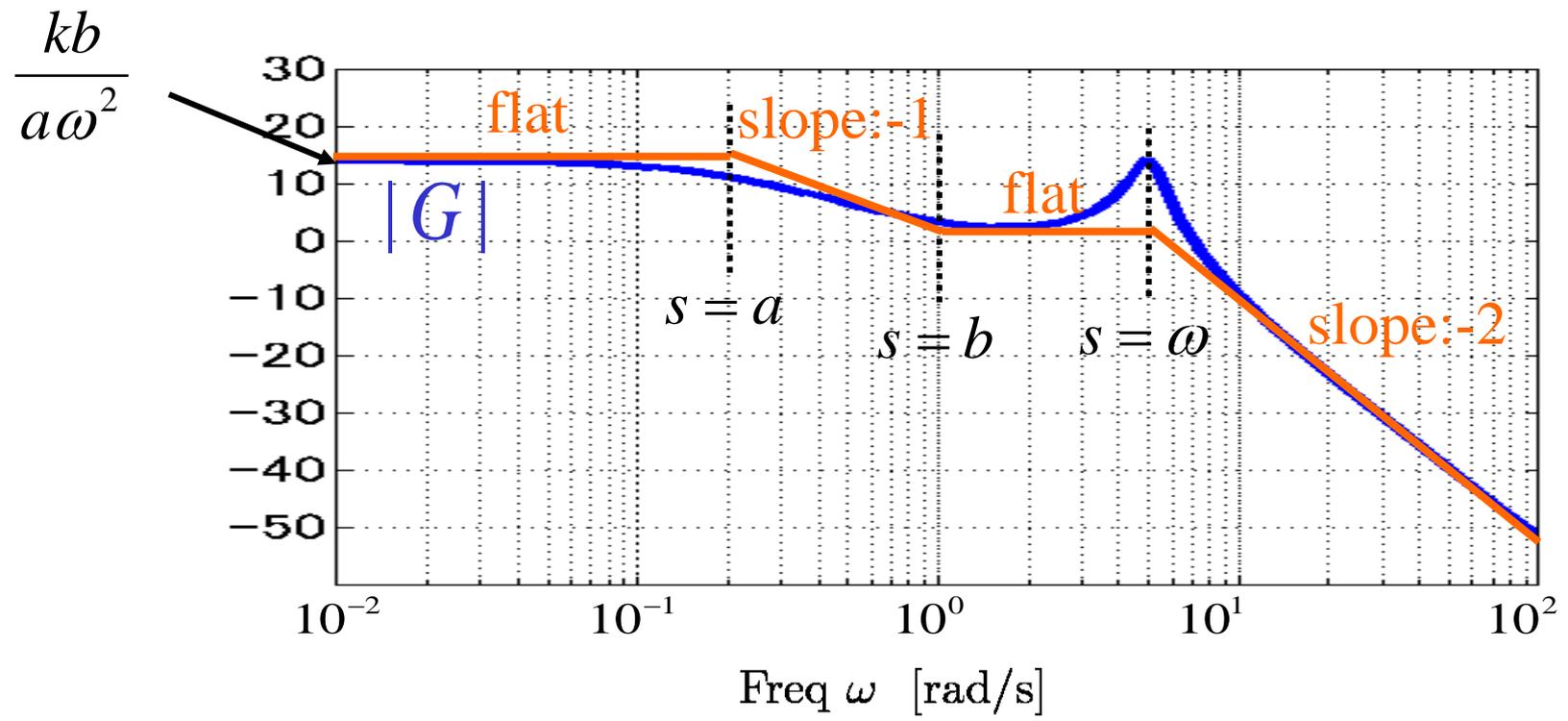
**Zero :**  $z = -2, 3.47$



**[Ex. 8.8]**

Process:  $G(s) = \frac{k(s+b)}{(s+a)(s^2 + 2\zeta\omega s + \omega^2)}$

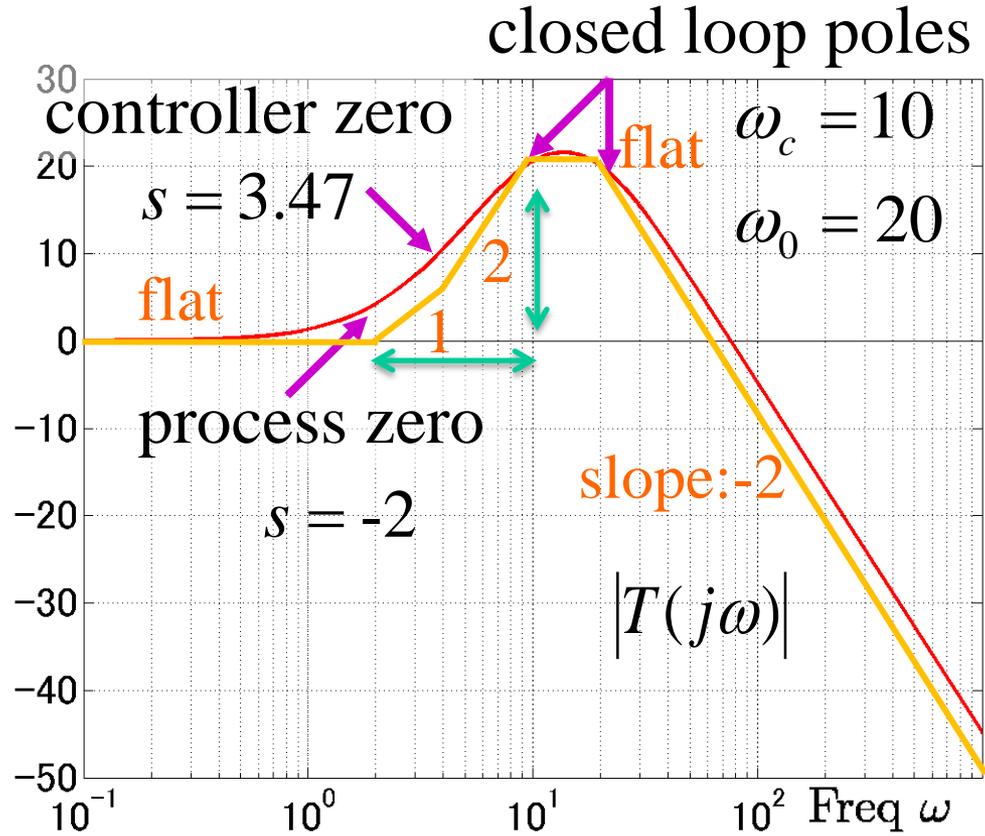
$a = 0.2, b = 1$   
 $\omega = 5, \zeta = 0.1$   
 $k = 25$



**Pole/Zero  $\iff$  Frequency Shape**

# [Ex. 12.8] Slow Stable Process Zeros

$$T = \frac{PC}{1+PC} = \frac{n_p n_c}{d_p d_c + n_p n_c}$$



**Pole** :  $-7.07 \pm 7.07i$  ( $\omega_c = 10$ )  
 $-14.14 \pm 14.14i$  ( $\omega_0 = 20$ )

**Zero** :  $-2, 3.47$

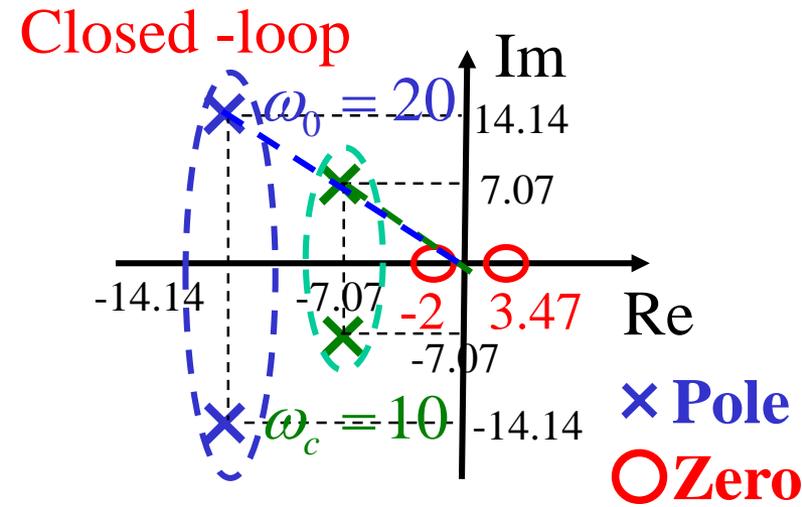


Fig. 12.12

The magnitude of the peak depends on the **ratio of the zeros and the poles** of the transfer function.

**assign a closed loop pole close to the slow process zero**

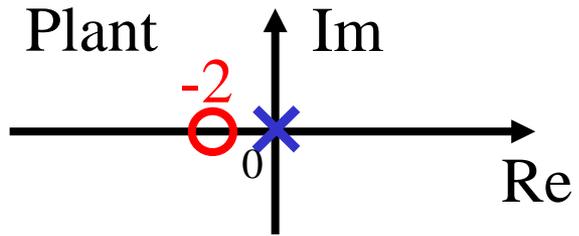
# [Ex. 12.8] Slow Stable Process Zeros

Process

$$P(s) = \frac{0.5s + 1}{s^2}$$

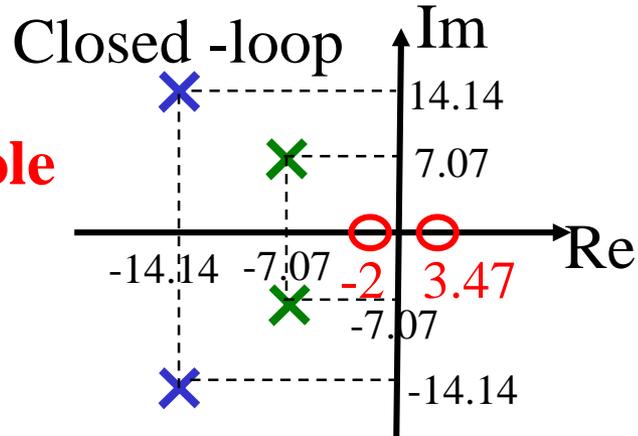
**Pole :**  $p = 0, 0$   
**Zero :**  $z = -2$

\*process stable zero  $z = \underline{-2}$



Faster close loop system

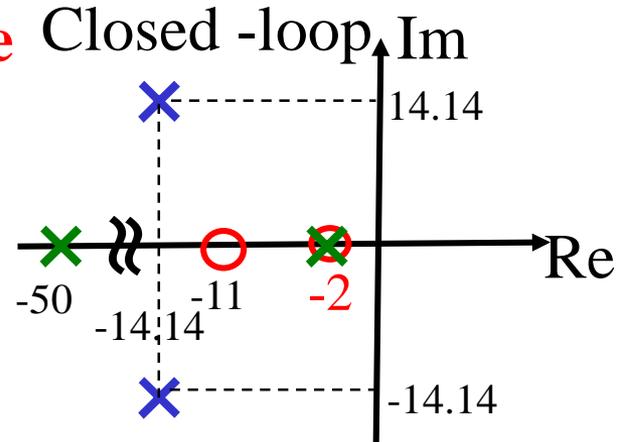
$$\left\{ \begin{array}{ll} \omega_c = 10 & \omega_0 = 20 \\ \zeta_c = 0.707 & \zeta_o = 0.707 \end{array} \right. \rightarrow \begin{array}{l} \text{closed loop pole} \\ -7.07 \pm 7.07i \\ -14.14 \pm 14.14i \end{array}$$



**Assign a closed loop pole close to the slow process zero.**

$$\left\{ \begin{array}{ll} \omega_c = 10 & \omega_0 = 20 \\ \zeta_c = 2.6 & \zeta_o = 0.707 \end{array} \right. \rightarrow \begin{array}{l} \text{closed loop pole} \\ -2, -50 \\ -14.14 \pm 14.14i \end{array}$$

$$\left( \begin{array}{l} \det(sI - A + BK) = s^2 + 2 \cdot 2.6 \cdot 10s + 10^2 \\ = (s + 2)(s + 50) \end{array} \right)$$



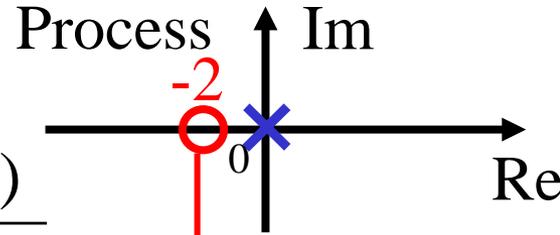
# [Ex. 12.8] Slow Stable Process Zeros

Process:  $P(s) = \frac{0.5s + 1}{s^2}$

$\omega_c = 10$   
 $\zeta_c = 2.6$

$\omega_o = 20$   
 $\zeta_o = 0.707$

$$C(s) = \frac{3628(s + 11.02)}{(s + 2)(s + 78.28)}$$



$$T(s) \approx \frac{1814(s + 11)(s + 2)}{(s + 2)(s + 50)(s^2 + 28s + 400)}$$

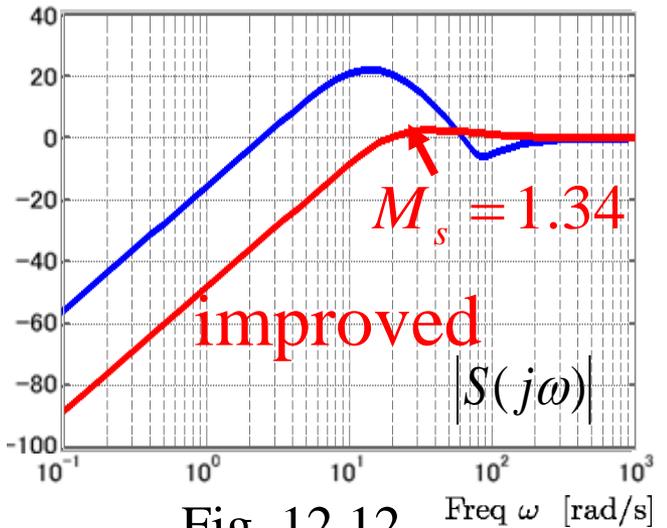
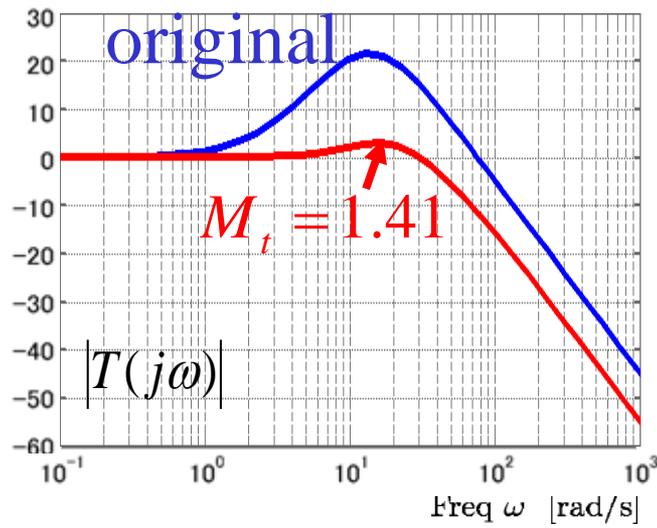
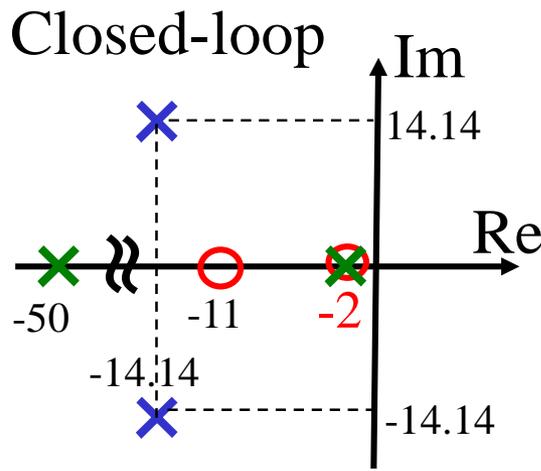
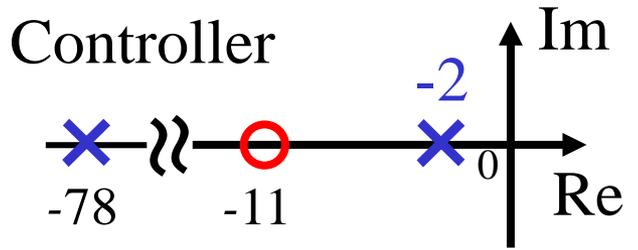


Fig. 12.12 Freq  $\omega$  [rad/s]

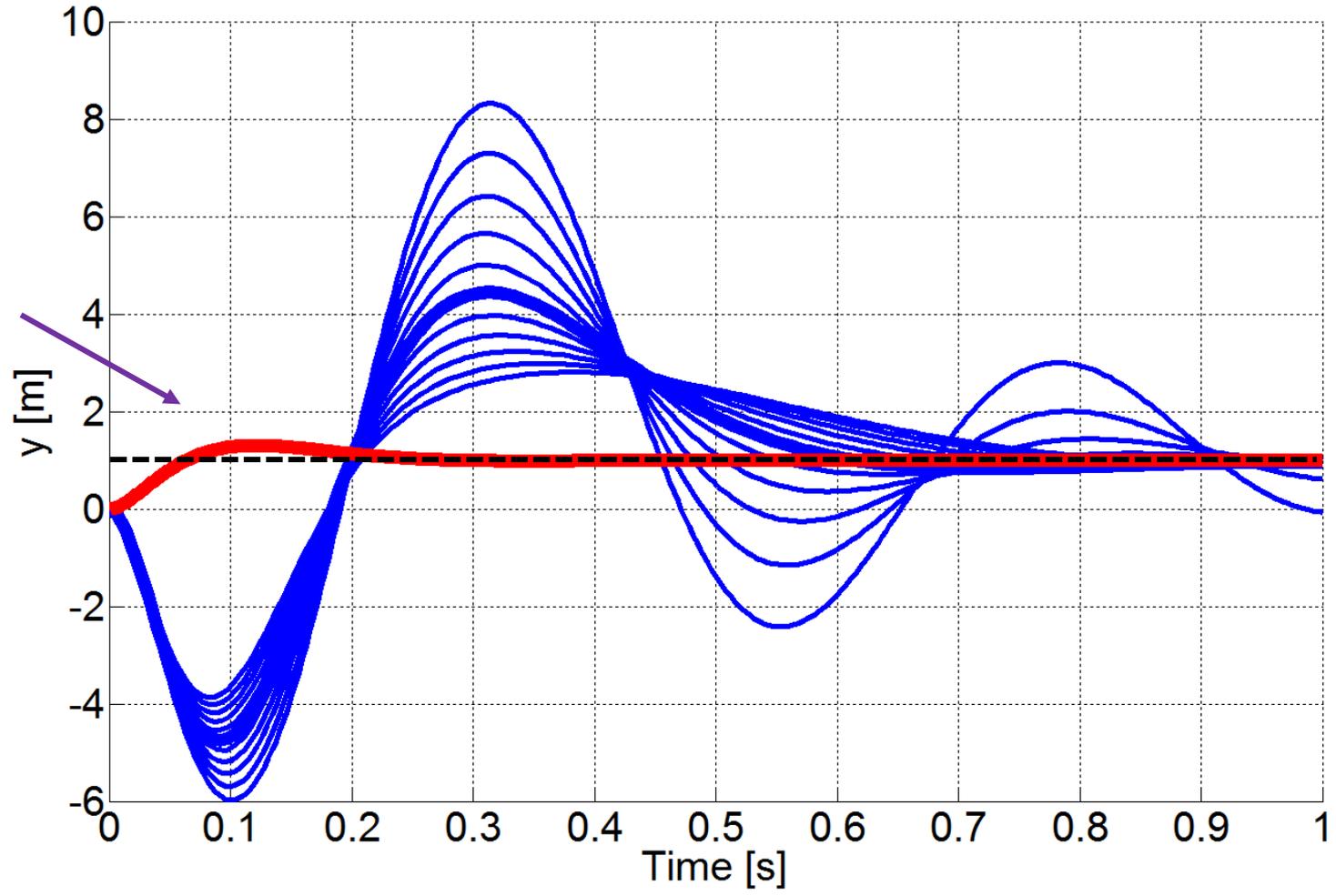
**Assign a closed loop pole close to the slow process zero**

# [Ex. 12.8] Slow Stable Process Zeros

$\omega_c = 10$	$\omega_o = 20$
$\zeta_c = 0.707$	$\zeta_o = 0.707$

$\omega_c = 10$	$\omega_o = 20$
$\zeta_c = 2.6$	$\zeta_o = 0.707$

2DOF controller



# [Ex. 12.9] Fast Stable Process Poles

Process

$$P(s) = \frac{b}{s+a}$$

**Pole :**  $p = -a$

PI controller

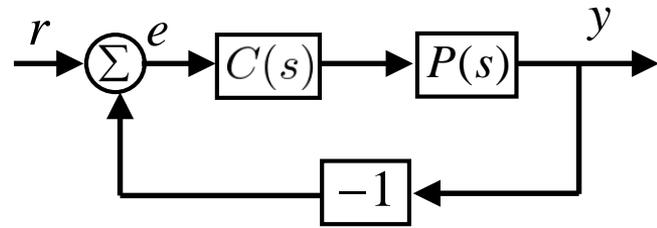
$$C(s) = \frac{k_p s + k_i}{s}$$

**Pole :**  $p = 0$

**Zero :**  $z = -k_i / k_p$

Loop transfer function

$$L(s) = \frac{b(k_p s + k_i)}{s(s+a)}$$



Closed loop characteristic polynomial

$$s(s+a) + b(k_p s + k_i) = s^2 + (a + bk_p)s + k_i b$$

↓ desired closed loop poles :  $-p_1 - p_2 \quad s^2 + (p_1 + p_2)s + p_1 p_2$

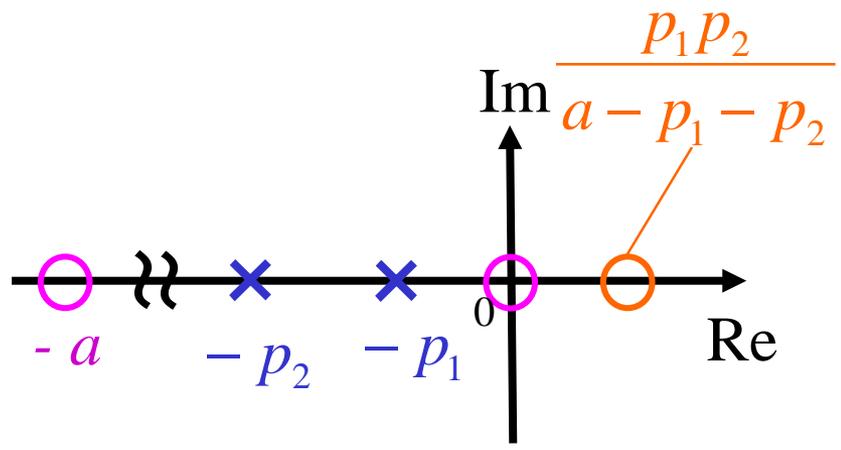
$$k_p = \frac{p_1 + p_2 - a}{b} \quad k_i = \frac{p_1 p_2}{b}$$

Complementary sensitivity

$$T(s) = \frac{(p_1 + p_2 - a)s + p_1 p_2}{(s + p_1)(s + p_2)}$$

Sensitivity

$$S(s) = \frac{s(s+a)}{(s+p_1)(s+p_2)}$$



assume  $p_1 < p_2 \ll a$

# [Ex. 12.9] Fast Stable Process Poles

assume  $p_1 < p_2 \ll a$

$$S(s) = \frac{s(s+a)}{(s+p_1)(s+p_2)}$$

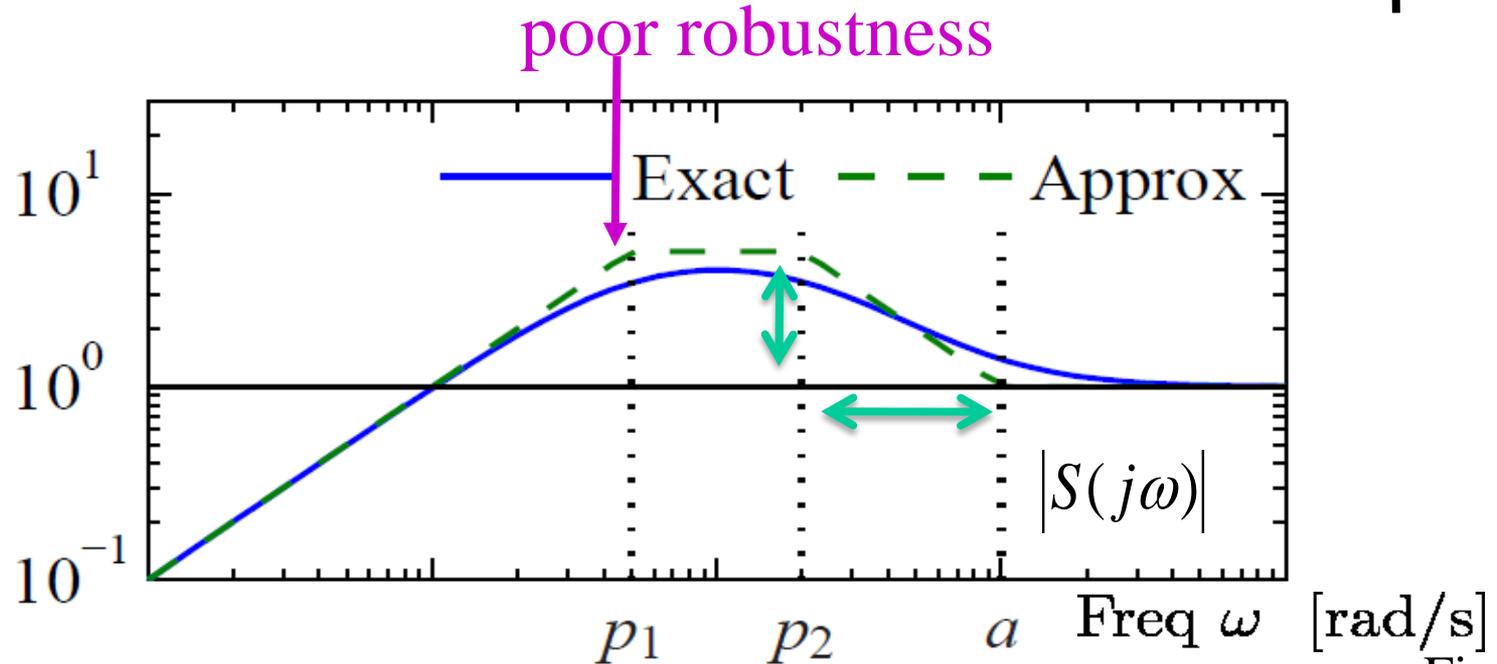
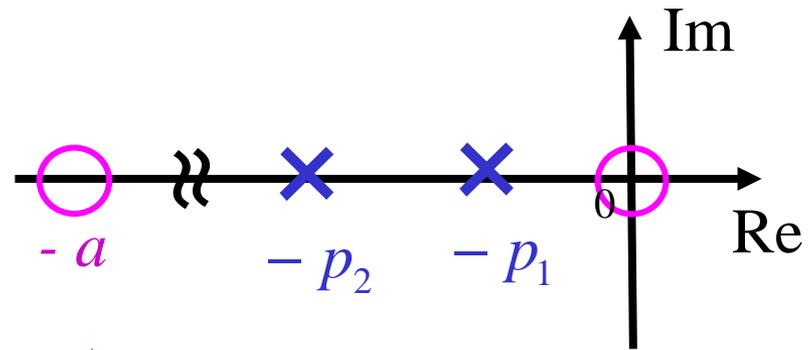


Fig. 12.13

Choose one closed loop pole equal to the process pole

$p_2 = a$

# [Ex. 12.9] Fast Stable Process Poles

Process

PI controller  $C(s) = \frac{k_p s + k_i}{s}$

Sensitivity

$$P(s) = \frac{b}{s+a}$$

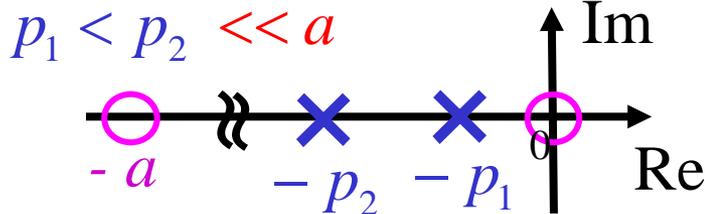
$$k_p = \frac{p_1 + p_2 - a}{b}, \quad k_i = \frac{p_1 p_2}{b}$$

$$S(s) = \frac{s(s+a)}{(s+p_1)(s+p_2)}$$

Pole :  $p = -a$

Pole :  $p = 0$

Zero :  $z = -k_i / k_p$



**Choose one closed loop pole equal to the process pole.**

$p_2 = a$

$$k_p = \frac{p_1}{b}, \quad k_i = \frac{a p_1}{b}$$

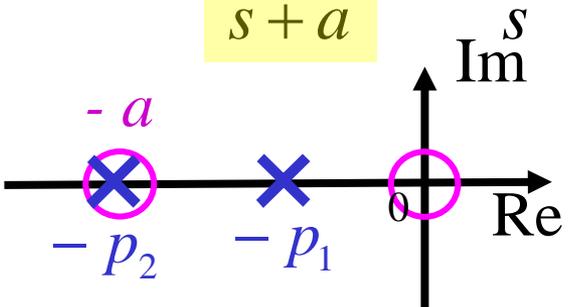
$$C(s) = \frac{k_p (s+a)}{s}$$

Pole :  $p = 0$

Zero :  $z = -a$

$$L(s) = \frac{b}{s+a} \cdot \frac{k_p (s+a)}{s} = \frac{b k_p}{s}$$

$$S(s) = \frac{s}{s + b k_p} \quad T(s) = \frac{b k_p}{s + b k_p}$$



The fast process pole is **canceled** by a controller zero

# [Ex. 12.9] Fast Stable Process Poles

Process  $P(s) = \frac{b}{s+a}$       PI controller  $C(s) = \frac{k_p(s+a)}{s}$

$$k_p = \frac{p_1}{b} \quad k_i = \frac{ap_1}{b}$$

**Pole :**  $p = -a$       **Pole :**  $p = 0$   
**Zero :**  $z = -a$

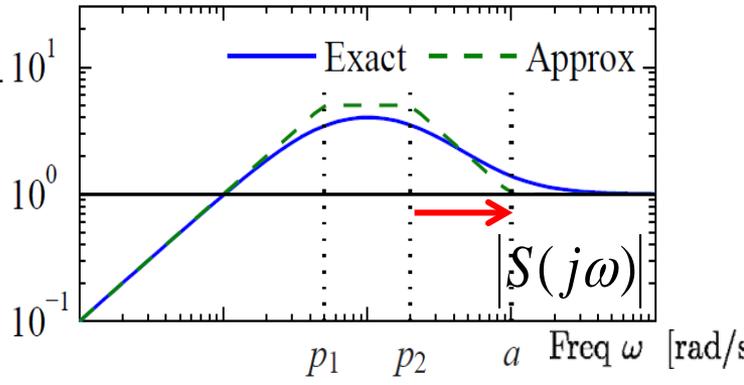
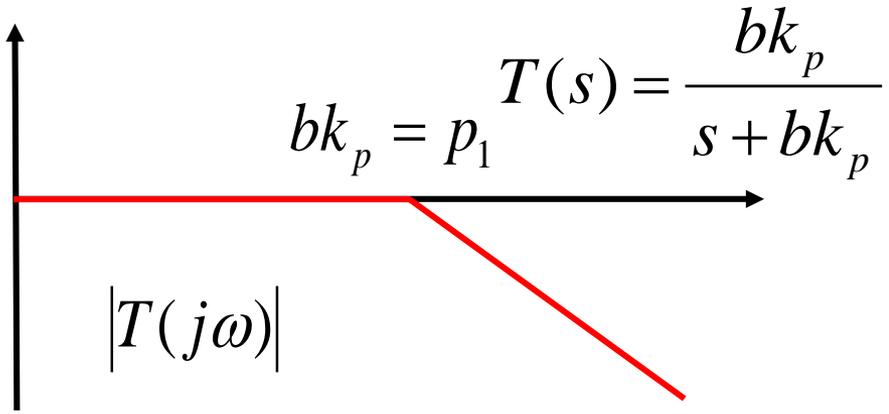
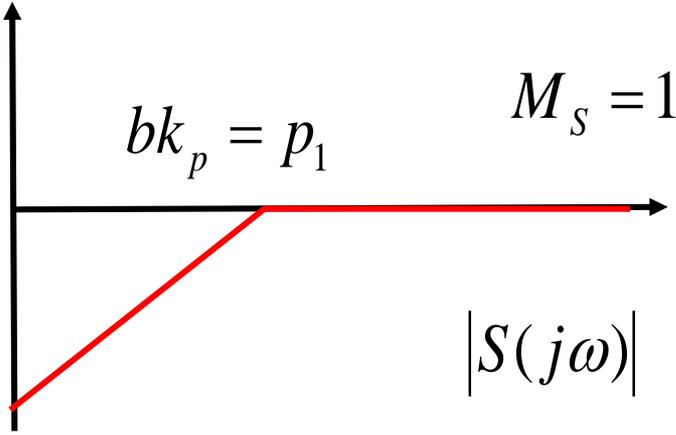
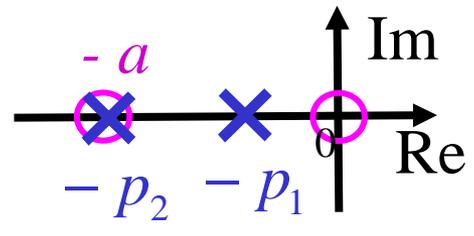


Fig. 12.13

## Sensitivity

$$S(s) = \frac{s(s+a)}{(s+p_1)(s+p_2)} \xrightarrow{p_2 = a} S(s) = \frac{s}{s+bk_p}$$



**Choose one closed loop pole equal to the process pole**

# 5th Lecture

## 12 Robust Performance

### 12.4 Robust Pole Placement: Examples

#### Example 12.8 (Slow Stable Process Zeros)

(pp. 362--364)

#### Example 12.9 (Fast Stable Process Poles)

(pp. 364--365)

**Keyword :** Robust Pole Placement,  
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